

Q.1a) kinematic viscosity = $\nu = 6$ stokes
 $= 6 \times 10^{-4} \text{ m}^2/\text{s}$

Sp. gravity = 1.6

$\therefore \rho = 1.6 \times 1000 = 1600 \text{ kg/m}^3$

$\nu = \frac{\mu}{\rho}$

$\therefore \mu = 6 \times 10^{-4} \times 1600$
 $= 0.96 \times 10 = \underline{\underline{9.6 \text{ poise}}}$

Q.2a) $a_1 = \frac{\pi}{4} d_1^2 = \frac{\pi}{4} \times 20^2 = 314.16 \text{ cm}^2$

$a_2 = \frac{\pi}{4} \times 10^2 = 78.54 \text{ cm}^2$

$P_1 = 17.658 \text{ N/cm}^2 = 17.658 \times 10^4 \text{ N/m}^2$

$\rho = 1000 \text{ kg/m}^3$

$\therefore \frac{P_1}{\rho g} = \frac{17.658 \times 10^4}{9.81 \times 1000} = 18 \text{ m of water}$

$\frac{P_2}{\rho g} = -30 \text{ cm of Hg} = -0.3 \times 13.6 = -4.08 \text{ m of water}$

$h = \frac{P_1}{\rho g} - \frac{P_2}{\rho g} = 18 - (-4.08)$

$= 18 + 4.08 = 22.08 \text{ m of water} = 2208 \text{ cm of water}$

$Q = C_d \times \frac{a_1 a_2}{\sqrt{a_1^2 - a_2^2}} \sqrt{2gh}$

$= 0.98 \times \frac{314.16 \times 78.54}{\sqrt{(314.16)^2 - (78.54)^2}} \sqrt{2 \times 9.81 \times 2208}$

$= \underline{\underline{65.555 \text{ lit/s}}}$

Q.3a) Section 1.

$$A_1 = 40 \text{ cm}^2 = 40 \times 10^{-4} \text{ m}^2$$

$$p_1 = 40 \text{ N/cm}^2 \text{ (gauge)}$$
$$= 40 + 10 = 50 \text{ N/cm}^2 \text{ (abs)}$$
$$= 50 \times 10^4 \text{ N/cm}^2$$

$$T = 15^\circ \text{C}$$
$$= 288 \text{ K}$$

$$R = 292 \text{ N}\cdot\text{m}/\text{kg}\cdot\text{K}$$

$$\frac{p_1}{S_1} = RT_1$$

$$\therefore S_1 = \frac{p_1}{RT_1} = \frac{50 \times 10^4}{292 \times 288} \frac{\text{kg}}{\text{m}^3} = 5.945 \text{ kg/m}^3$$

$$\text{mass flow rate} = S_1 A_1 V_1 = 0.5$$

$$0.5 = 5.945 \times 40 \times 10^{-4} \times V_1$$

$$\therefore V_1 = 21.02 \text{ m/s}$$

For isothermal process, T is const.

$$\therefore T_2 = 288 \text{ K}$$

$$\frac{p_2}{S_2} = RT_2 \dots$$

$$S_2 = \frac{40 \times 10^4}{292 \times 288} = 4.756 \text{ kg/m}^3$$

$$\text{mass flow rate} = S_2 A_2 V_2 = 0.5 = 4.756 \times 20 \times 10^{-4} \times V_2$$

$$\therefore V_2 = 52.565 \text{ m/s}$$

Q.4b) Case I:

$$P_1 = \text{power required} = 12 \text{ hp}$$

$$\dot{m}_1 = \text{feed rate} = 15 \text{ T/hr.}$$

$$D_{s_{a1}} = \text{vol. surface mean dia. of feed} = 0.75 \text{ inch.}$$

$$D_{s_{b1}} = \text{vol. surface mean dia. of product} = 0.2 \text{ inch.}$$

[P.T.0]

③ Case II

$$P_2 = ?$$

$$m_1 = 10 \text{ T/hr}$$

$$D_{sa2} = 0.75 \text{ inch}$$

$$D_{sb2} = 0.2 \text{ inch}$$

Rittinger's law.

$$\frac{P}{m} = k_r \left[\frac{1}{D_{sb}} - \frac{1}{D_{sa}} \right]$$

k_r : Rittinger's constant.

$$\therefore \frac{\frac{P_1}{m_1}}{\frac{P_2}{m_2}} = \frac{\left[\frac{1}{D_{sb1}} - \frac{1}{D_{sa1}} \right]}{\left[\frac{1}{D_{sb2}} - \frac{1}{D_{sa2}} \right]}$$

$$\frac{12/15}{P_2/10} = \frac{1/0.2 - 1/0.75}{1/0.15 - 1/0.75}$$

$$\therefore P_2 = 11.64 \text{ hp}$$